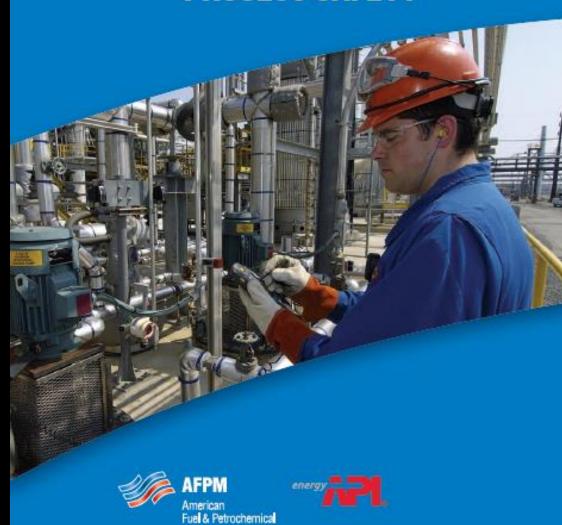
ANSI API RP-754Quarterly Webinar

February 16, 2016

Process Safety Performance Indicators for the Refining and Petrochemical Industries

AFPM & API ADVANCING PROCESS SAFETY



Purpose of RP 754 Quarterly Webinars

- To support broad adoption of RP-754 throughout the Refining and Petrochemical industries
- To ensure consistency in Tier 1 and 2 metrics reporting in order to establish credibility and validity
- To share learning's regarding the effective implementation of Tier 1-4 lagging/leading metrics

Today's Agenda

- Introductions Kelly Keim, ExxonMobil
- CY 2015 Collection
 - Deadline
 - Reminder on Public Reporting
 - Overview of submission spreadsheet updates, QA tab, and common mistakes
- Status ANSI API RP-754 2nd Edition
- 2016 Webinar Dates

CY 2015 PSE Data Collection

 Data Collection began January 2015 for CY 2015 PSE Submissions

- HARD DEADLINE March 18, 2016
 - We will not accept data after this date, no exceptions
 - Purpose is to begin QAQC process in order to finalize reports by mid-summer
- Reminder:
 - "Company transparent" PSE data will NOT be published in their reports or on their websites

...what does this mean for your company?

ANSI API RP 754 – Public Reporting Requirements

- To be in compliance with RP-754 companies "shall" report Tier 1 and Tier 2 PSE rates in a nationwide, broadly accessible way.
- Options include:
 - Company-specific reports or websites
 - Industry Association or Professional Society reports or web sites
 - Government Agency or Other Organizations
 - Text from the standard is located in the back-up sldies

Common PSE Submission Errors

- Reminder; please take time to submit good descriptions for each event. Examples of good and bad submissions are in the back-up slides
- Column AD Employee Days Away from Work Injuries
 - We are looking for the # of Cases resulting from Days Away from Work, not the # of Days
- Facility Information Make sure you display the site name from "Facility Information" to the "Event Consequence" tab exactly the same, do not use abbreviations

Common PSE Submission Errors

- Only list both Tier 1 and Tier 2 consequences when there are injuries to report.
- Double check the Tier 1 and 2 designation by using the "Summary" tab, we commonly see that companies make an error and do not notice it until the data is aggregated in the Final Report.
- If you indicate a release occurred, make sure you chose a release category
- Double check man hours are accurate, especially for contractors
 - We still get companies that do not enter in Contractor hours, make sure your submissions are complete

Status – ANSI API RP-754 2nd Edition

- First ballot was overwhelmingly accepted
- Second ballot approved and finalized
- Document has been submitted to ANSI
- Final document to be published in March or April

Webinar Dates

- March 22 11:00 am Eastern
- May 17 Presentations at AFPM National Occupational & Process Safety Conference on API RP 754, Rev. 2 – San Antonio, Texas
- June 21 11:00am Eastern
- September 13 11:00 am Eastern
- December 13 11:00 am Eastern

2015 Tier 1 and Tier 2 PSE data submittals

Contacts:

<u>API:</u>

- Email spreadsheet directly to Hazem Arafa at <u>arafah@api.org</u> or,
- Load data into API PSE portal located at https://pseportal.api.org/

AFPM:

- Email spreadsheet directly to Anna Scherer at safetyportal@afpm.org or,
- Load data into AFPM Process Safety Metrics portal located at <u>AFPM Safety Portal</u>

Resources

- API
 - API RP 754 Fact Sheet
 - Series of four webinars presented in fall 2010 (available for viewing)
 - Listing of FAQ's that help you properly classify a PSE
 - API Guide to collecting PSE data
 - Read-only access to API RP 754
 - Contact Ron Chittim at chittim@api.org for more information
 - Website: http://www.api.org/environment-health-and-safety/health-safety/process-safety-industry/measuring-safety-improvement.aspx
- AFPM Safety Portal
 - Process Safety metrics searchable database
 - 2011-2013 annual Process Safety Event reports
 - AFPM Guide to reporting PSE data
 - A "Hypothetical Process Safety Metrics Story"
 - Website: http://safetyportal.afpm.org/ProcessSafetymetrics-access.aspx

BACK UP SLIDES

10.3 Stakeholder

10.3.1 Broad Access (Nationwide) Public Reporting

Annually, each Company shall publicly report Tier 1 and Tier 2 PSE information specified in Table 3. It should also include other appropriate information based upon the data capture specified in 10.4. The information should be continuously available for at least five years.

Reporting may be directly from an individual company or through industry trade groups, government agencies or other means. Options for public reporting include:

- a) Company Specific Reports or Web Sites—When reporting information directly to the public or to other interested parties, Companies may make PSE information readily available on a publicly accessible web site, or as a written report provided upon request by any interested party.
- b) Industry Association or Professional Society Reports or Web Sites—API, ACC, NPRA, CCPS, UKPIA, or other petroleum or petrochemical industry associations may collect and report Tier 1 and Tier 2 PSE information. These reports may be in the form of publicly accessible web sites, or as written reports provided upon request by any interested party. The advantage of association or society reporting is that it allows interested parties to view information in one place and enables benchmarking of performance.
- c) Government Agency or Other Organizations—Local, state, or national government agencies, or other organizations may elect to establish reporting web sites.

Table 3—Stakeholder Report Information

		Industry	Company
Tier 1	PSE Count	X	See Note
	PSE Rate	Х	Х
Tier 2	PSE Count	Х	See Note
	PSE Rate	Х	Х

NOTE Comparisons among companies and industries are only statistically valid on a rate basis; therefore, Company PSE counts are not reported publicly.

10.3.2 Local (Site) Public Reporting

Each Company's site should determine the appropriate methods to communicate PSE information to its employees and employee representatives, the local community, and emergency management officials.

Annually, each Company's site shall report a summary of its site-specific Tier 1, 2, 3, and 4 PSE information to its employees and employee representatives. Unattended, remote-operated or single-manned facilities are exempt from this requirement.

Annually, each Company's site shall make available a summary of site-specific Tier 1 and 2 PSE information and can report site-specific Tier 3 and 4 PSE information to the local community and emergency management officials along with information regarding measures taken to improve performance. This includes any communities that could reasonably be affected by a LOPC event. Remote sites where the worst potential-case LOPC cannot impact any public receptors are exempt from this requirement.

- The three "Big Items":
 - \$25k or \$100k Tier 1 direct cost limit for fire or explosion damage Result: Super majority "approved" increase to \$100,000; Tier 2 is \$2,500 \$100,000.
 - Mandatory or optional use of Tier 1 severity weighting
 Result: Optional but data (i.e. total severity number per event)
 will be requested by API/AFPM
 - Tier 1 and Tier 2 threshold release categories and quantities (GHS v. non-GHS)

Result: Super majority "approved" non-GHS option

^{*} The user is cautioned to refer to the final published ANSI API RP-754, Second Edition to ensure complete and accurate information.

- Applicability Addition of <u>informative annexes</u> for the application of RP-754 to Petroleum Pipelines & Terminals, Retail Service Stations, and Oil & Gas Drilling and Production Operations
- Applicability Clarified that routine emissions from permitted or regulated sources are still out-of-scope, however <u>upset emissions</u> are evaluated for Tier 1 or Tier 2.

...an upset emission from a permitted or regulated source, of a quantity greater than or equal to the threshold quantities in Table 1 (Tier 1) or Table 2 (Tier 2) in any one-hour period, that results in one or more of the following four consequences:

- rainout;
- discharge to a potentially unsafe location;
- an on-site shelter-in-place or on-site evacuation, excluding precautionary on-site shelter-in-place or on-site evacuation;
- public protective measures (e.g., road closure) including precautionary public protective measures.

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Definitions -

- <u>Active Staging</u>: Clarification concerning when truck or rail car exit their transportation mode. <u>Active staging is part of transportation</u>.
- <u>Active Warehouse</u>: On-site warehouses that store raw materials, intermediates, or finished products used or produced by a refinery or petrochemical facility are part of the process
- <u>Alternate Primary Containment</u>: The Tier 1 and Tier 2 threshold quantity consequence is excluded for releases to alternate primary containment.

Tier 1 -

- Added a threshold release quantity for UNDG Class 2, Division 2.2 (non-flammable, non-toxic gases; i.e. asphyxiants/oxidizers) excluding air
- Changed the indoor threshold release quantity from 50% to 10% of the outdoor release quantity
- Changed the fire and explosion direct cost threshold from \$25,000 to \$100,000

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Tier 2 -

- Added a threshold release quantity for UNDG Class 2, Division 2.2 (non-flammable, non-toxic gases; i.e. asphyxiants/oxidizers) excluding air
- Aligned the Tier 1 and Tier 2 threshold release categories
- Added an upper bound on high flash materials released below their flashpoint [93 °C (200 °F)]

Additional PSE clarifications –

- A pressure relief device (PRD), safety instrumented system (SIS), or other engineered depressuring device discharge is an LOPC due to the unplanned nature of the release
- An internal fire or explosion that causes a LOPC from a process triggers an evaluation of the Tiered consequences. The LOPC does not have to occur first
- an officially declared community evacuation or community shelter-inplace includes precautionary evacuation or shelter-in-place

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- PSE Data Capture
 - a. Added a list of petrochemical process units
 - b. Added subcategories for the normal mode of operation
 - c. Added a list of causal factors
- Tier 1 PSE Severity Weighting Added an informative annex for calculating the severity weighting of Tier 1 Process Safety Events
- PSE Examples Added a significant number of new examples of the informative annex

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- Multicomponent Releases Added an informative annex to provide guidance on the determination of threshold release quantities for multicomponent releases
- Addition of an informative annex to provide guidance for the implementation of Tier 3 and Tier 4 indicators
- Addition of an informative annex for Tier 4 example indicators

Incident Descriptions that are not helpful:

 Examples of incident descriptions that are not helpful for data analysis (i.e., need to be expanded)

Loading Rack Spill

Pipeline Leak

Fire on E-1 Exchangers

Sump vent stack vapors

Tank 143 overfill

Piping failure on west Tk-52 pump.

Charge tank was overfilled

Others leave you wondering if the incident was even a Tier 1 or 2 event.

Power grid shut down resulting in loss of vapor recovery systems

Flared hydrogen sulfide as a result of a unit shutdown

Better, but could be improved with a little more detail

Hydrogen Sulfide was released due to a tubing fitting leak on the Hydrogen Recycle Compressor's discharge flow transmitter.

Why did the fitting leak?

LOPC on tank mixer packing due to loss of lubrication caused by continued use below the minimum level for mixer operation.

Why operated too low?

1" bleeder broken on exchanger head causing an LPG release and fire.

How was it broken?

Some were really good

A flash fire occurred in the FCC reactor when contractor employees were pulling the spectacle blind to change new gaskets on the blind. The Main Column was lined to the flare and flare gas flowed through backwards up the vapor line into the reactor catching fire. The flash fire resulted in one contractor employee receiving minor burns.

Leak on a fractionator Reflux line located in the pipe rack due to corrosion. Corrosion was caused from a leak in a process water line dripping on the reflux line. The Reflux pump was shut down and the line was isolated.

Crane struck crude unit piping at the desalter while removing sump pump.
There was a crude release which found an ignition source resulting in a minor fire.

LOPC from overfilling small caustic tank due to malfunctioning level indication and backflow.

Leak on distillate line caused by corrosion/erosion.

These offered both consequence(s) and a cause

Conclusion

- More detailed incident descriptions will help the annual industry data analysis.
- Please share this presentation with those in your company who submit data.
- Special note: International sites had especially short descriptions of 2013 data.
- Recommendation: Have one person in the company review all PSEs prior to submittal and expand on the descriptions where possible.